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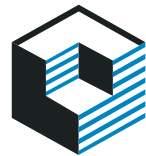
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The Wonderful World of Pneumatic Conveying

It Will Blow You Away.....



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Goals for Today!

- **Develop:**
 - *General understanding of pneumatic conveying systems and equipment*
 - *Understanding of a typical plant's transfer system*
 - *Troubleshooting skills for fines and streamers issues*

“We create sustainable business value by being a preferred solutions provider to our customers.”

Agenda

- **Types of Flow: Dilute vs. Dense Phase**
- **How fines and streamers are generated**
- **System components**
- **System design best practices**

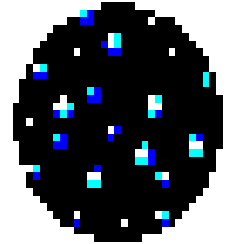
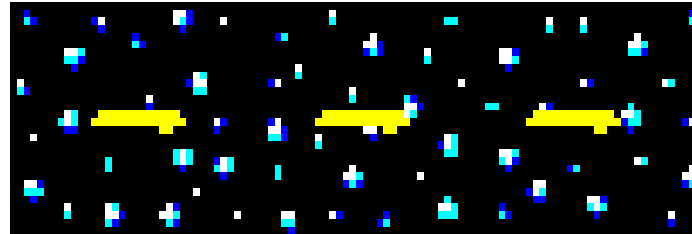
What is Pneumatic Conveying?

- **Moving objects with air**
 - ***Vacuum - Pulls***
 - System pressure is less than atmospheric
 - *Vacuum Cleaner*
 - *Drinking Straw*
 - ***Pressure - Push***
 - System pressure is greater than atmospheric
 - *Leaf Blower*
 - *Garden Hose*

Dilute vs. Dense Phase...

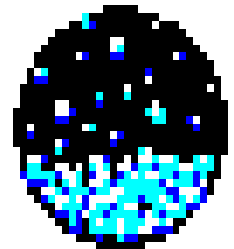
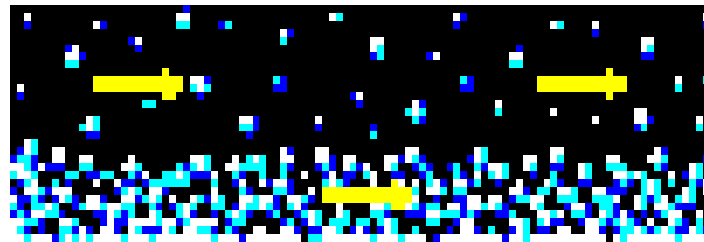
- **Stream Flow (Dilute)**

- air/solids > 2.25



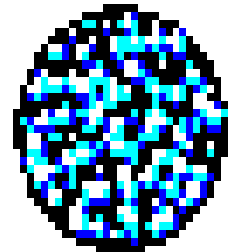
- **Two Phase Flow**

- $2.25 < \text{air/solids} < 0.2$



- **Pulsed Piston Flow**

- air/solids < 0.2



**loadings ratio in units of scf of air/lbs of pellets*

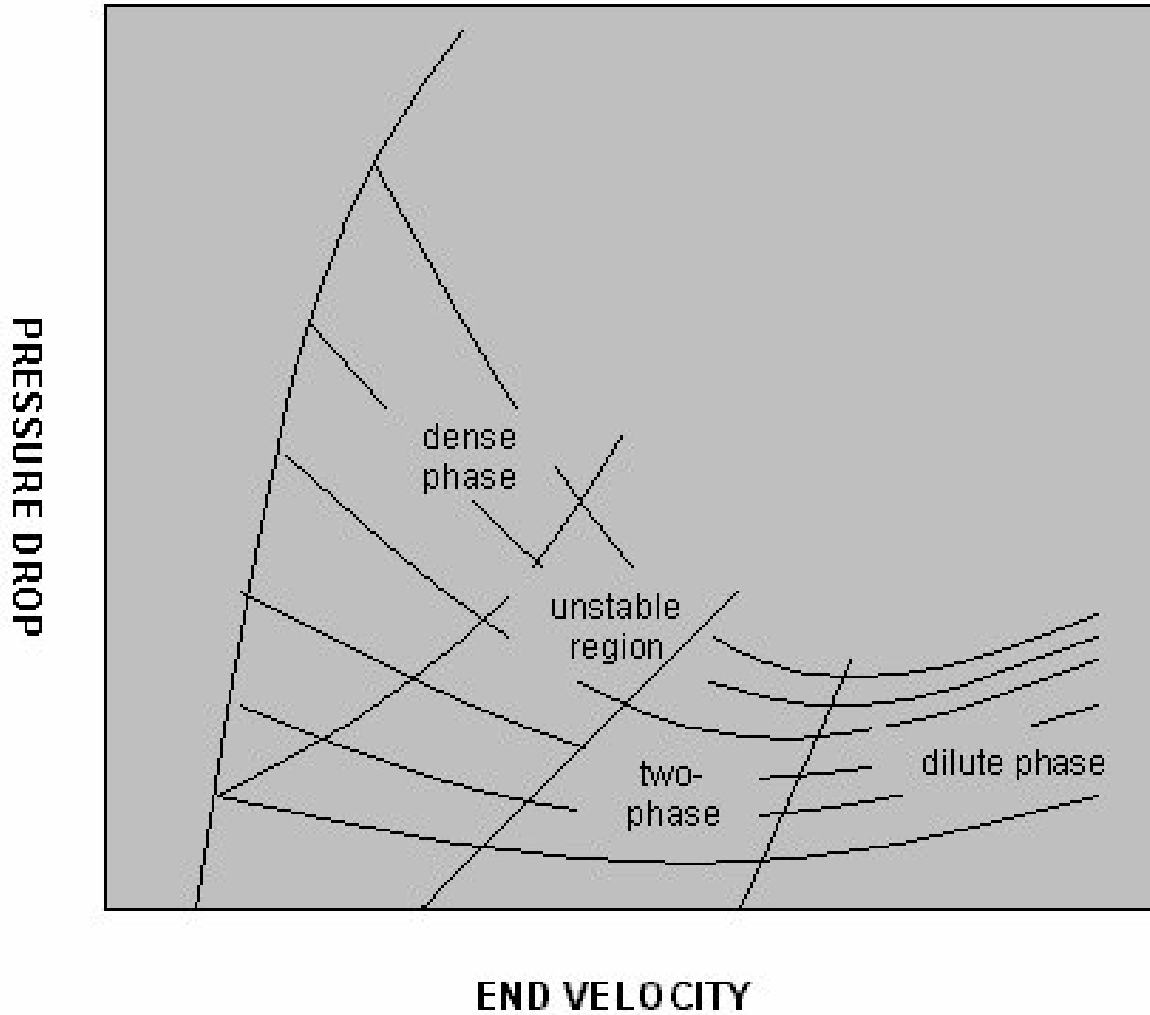
Dilute Phase Conveying

- Object are suspended in the conveying air
- The transfer velocity is greater than the “saltation” velocity
- Low system pressures (< 14 psig)
- High air to solids loading ratios (> 2.25)
- High linear velocities (4,200 – 6,500 ft/min)
- More destructive - mostly due to the high velocities
- Lower capital costs at startup
 - *Lower cost equipment / not rated for pressure system*
- Easier to operate
 - *Wider Δv range on phase diagram*

Dense Phase Conveying

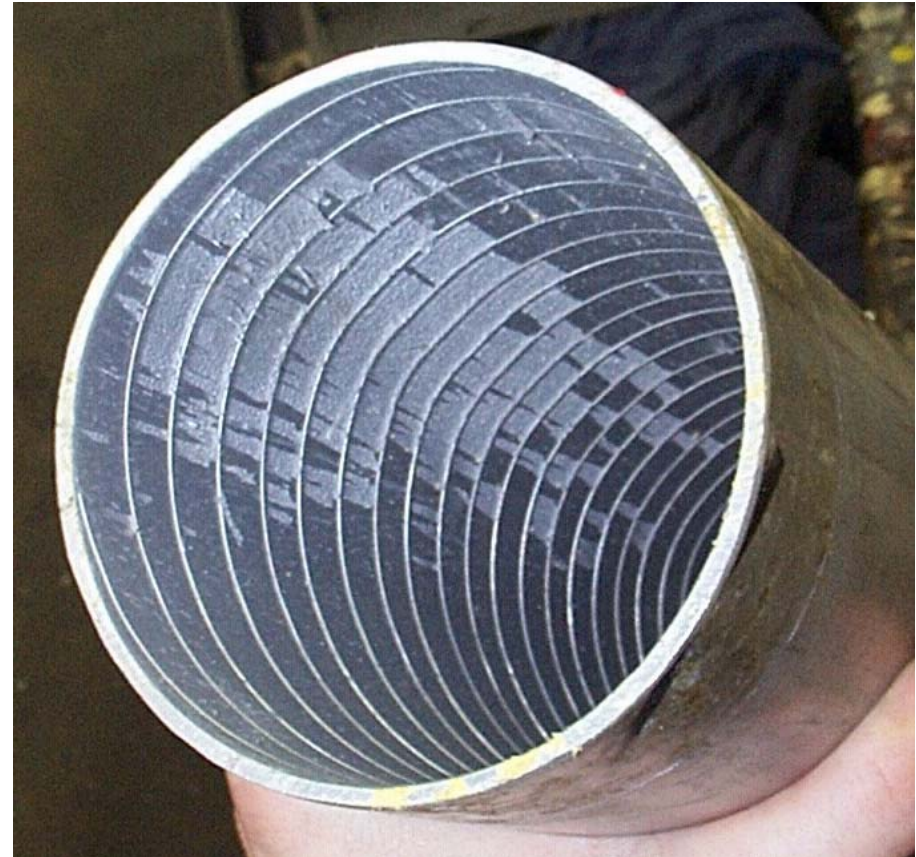
- Anything that is not Dilute Phase
- The transfer velocity is less than the “saltation” velocity at some point in the system (< 4,200 ft/min)
- High system pressures (14 – 90 psig)
- Low air to solids loading ratios (< 0.2)
- Low velocities but high pounds capacity (10^1 – 10^2 ft/min)
- Less destructive – a result of lower velocity
- Higher capital costs at startup
 - *Pressure rated lines, airlocks, valves, etc.*
- More difficult to operate (easier to plug)
 - *Narrower Δv range on phase diagram*

Pneumatic Conveying Phase Diagram

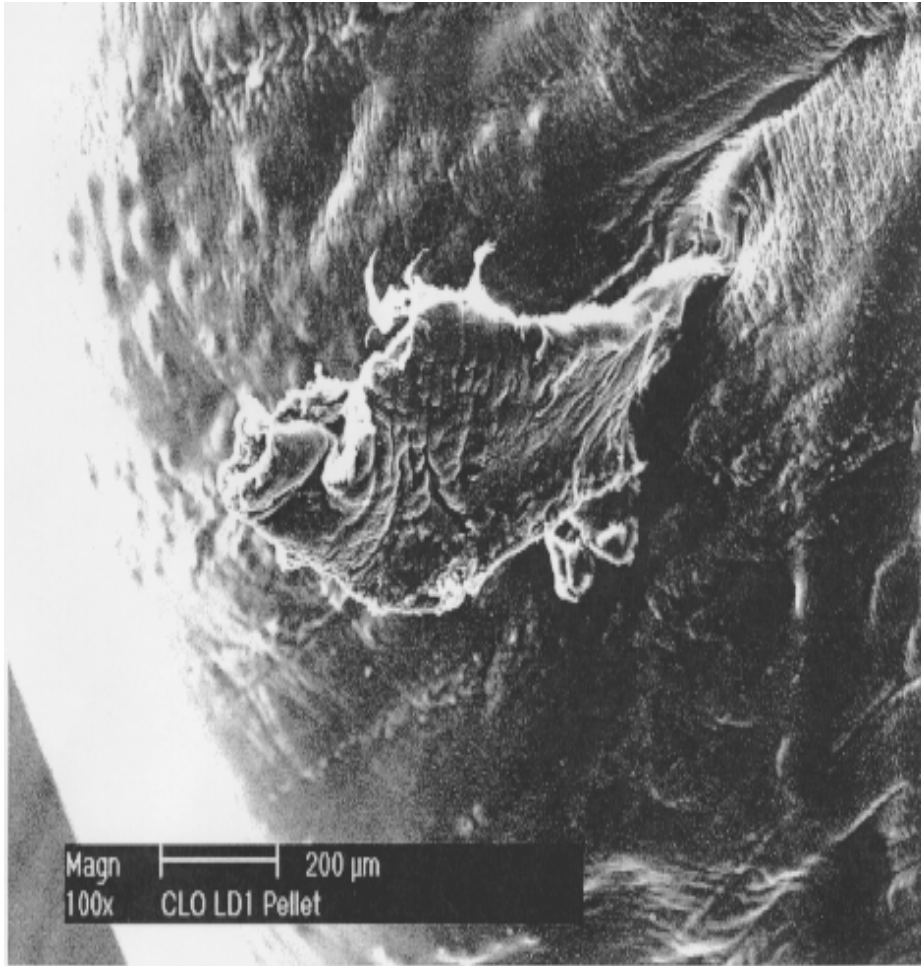


The Origin of Fines and Streamers

- A coating of plastic formed by smearing pellets against the pipe wall
- Skin peels off in strips and becomes streamers, angel hair, and/or fines



Pellet Tail Can Form Fines



- Tails are small stubs of polymer that are the result of poor pellet cut
- Pellet tails can break off and generate fines
- Small percentage of fines studied looked like pellet tails (<7%)

Fines Are “Mini-Streamers”



- Most fines look like “mini-streamers” under a microscope
- Most fines are generated by “smearing” and not tails.
- Breaking up of snakeskins forms angel hair and fines

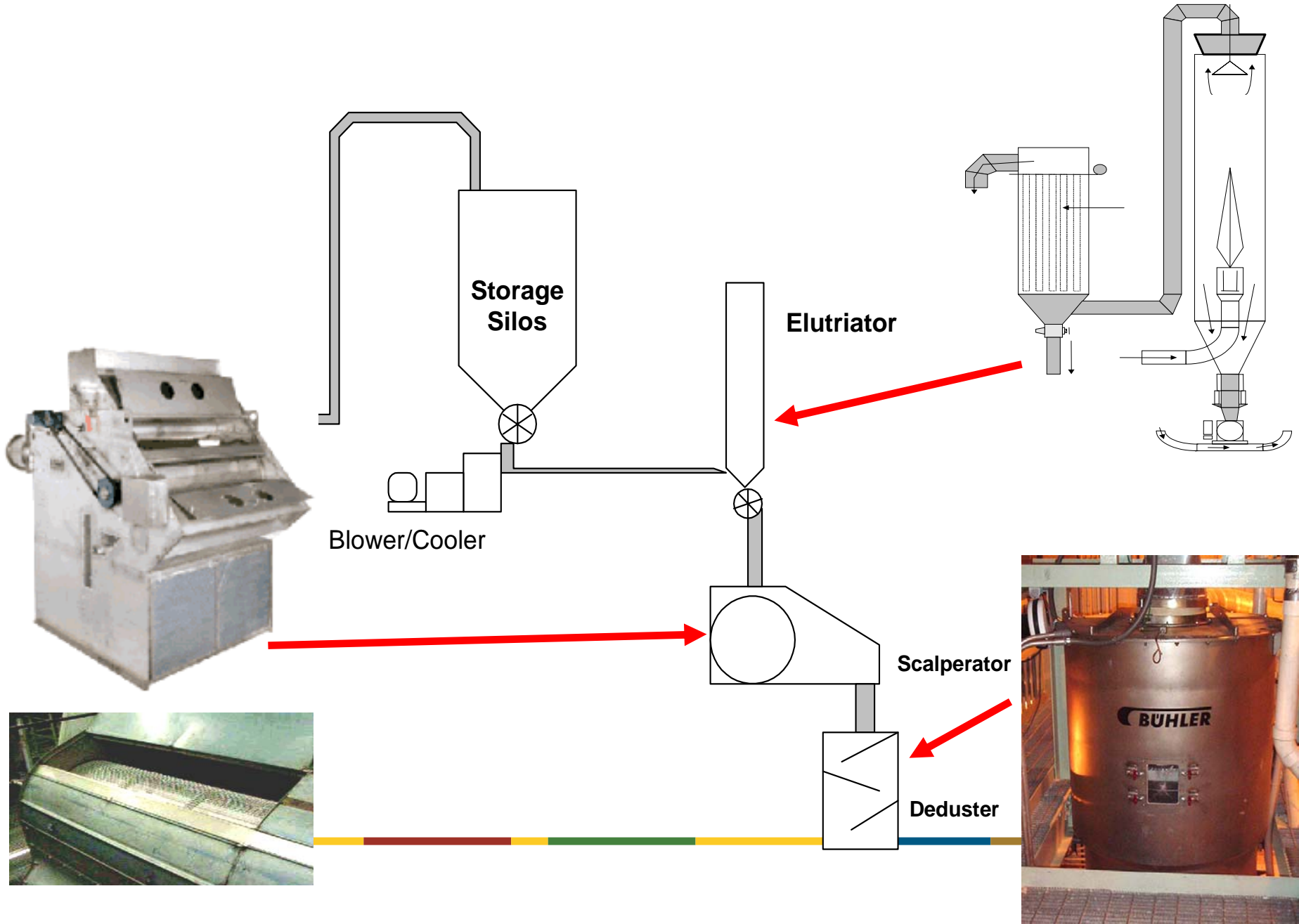
Typical Conveying System

- **Feed Vessel**
- **Feed Point**
 - *Pressure System: Air Lock (rotary valve)*
 - *Vacuum System: Gate Valve*
- **Air Mover (Blower)**
 - *Pressure: Mover at the solids pickup*
 - *Vacuum: Mover at discharge vessel*
- **Air Cooler**
 - *Located at the blower discharge*
 - *Especially a concern with pressure systems due to temperature rise induced by the blower*

Typical Conveying System-Continued

- **Transfer line**
 - *including piping, elbows, and divert valves*
- **Discharge vessel**
 - *Feed hopper at the extruder*
- **Particulate removal equipment**
 - Bag filters (suction of vacuum blowers)
 - Dedusters-fines
 - Elutriators-some fines and streamers
 - Scalperators-streamers
 - Cyclones
 - *tangential entry vessels can be conducive to streamers generation*

Typical Pellet Transfer System



The Common Elbow

- **Long Radius Bends**

- ***Lowest $-\Delta P$***

- among all bends***

- ~20 ft of straight pipe

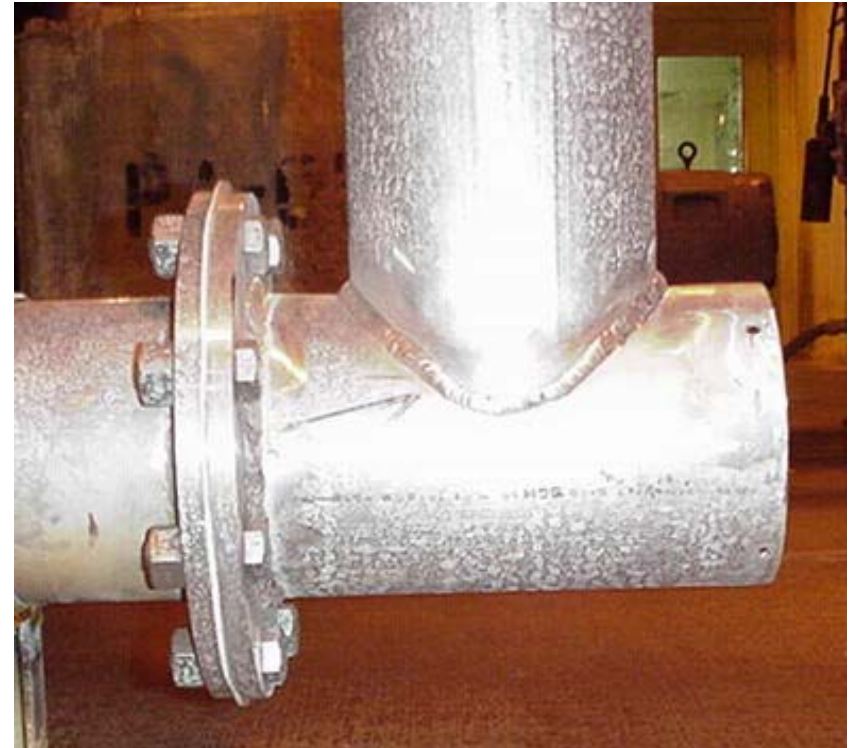
- ***Generates Streamers***

- Pellets “smear” against the outermost wall of the elbow
 - Frictional heat generated by this rubbing causes the outer portion of the pellet to melt and leave a skin
 - This skin peels off as snakeskins and could potentially be broken into angel hair/fines



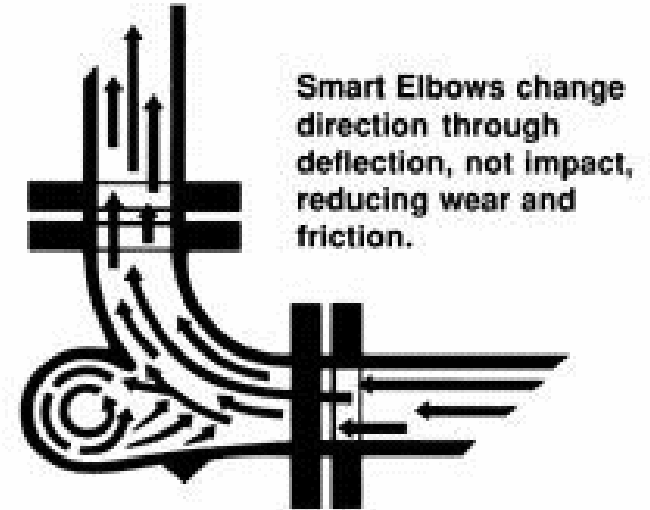
Dead End Tees

- Largest $-\Delta P$ among all bends
 - *~70 ft. of straight pipe*
- Minimizes streamers
 - *Semi-static bed of pellets forms in dead end and acts as a cushion*
- Vortex in bed provides for self cleaning
 - *Tee wears out if pocket is not formed due to low solids/air ratio*
- Least expensive of specialty bends
- Easy to fabricate



Hammertek Smart Elbow

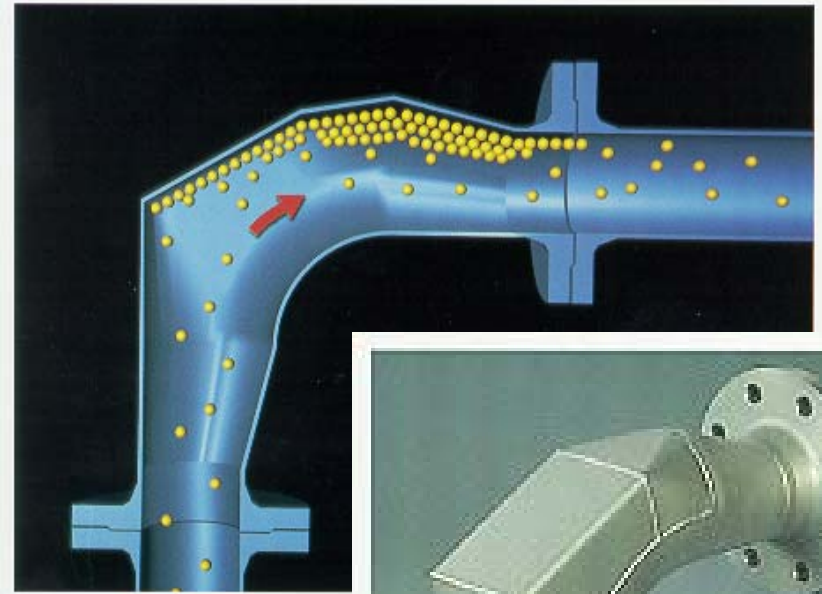
- $-\Delta P$ similar to long radius
- *Minimizes wear*
- *Minimizes streamers*
 - Circulating bulb of pellets deflects the solids



Specialty Elbows

■ Coperion Gamma Bend

- *$-\Delta P$ is less than DET but greater than LR*
- *Minimizes streamers*
 - Moving bed of pellets minimizes impact



Specialty Elbows

■ Diamond Cut

■ *$-\Delta P$ similar to short radius*

- greater than long radius bends
- similar/slightly less than DET

■ *Minimizes streamers*

■ *Streamers prevented from Diamond Cut on inner wall*

- Fines generation is still an issue—smearing mechanism of pellets to metal is still present



Specialty Piping

■ Shot Peened

- *Shot is used to roughen the inside of the transfer pipe*
- *The roughening of the pipe prevents the formation of snakeskins*
- *More fines are generated due to abrasion*
- *Helps with reducing large snakeskins but generates more fines*
- *Inexpensive initial cost, but has a short life span*

Specialty Piping

- **Spiral Grooved**

- *A lip is machined into the inner wall of the pipe*
- *Groove acts as a “speed bump” and prevents the pellets from smearing*
- *Expensive initial cost*
- *Has a substantially longer lifespan than peening*

Ideal Pneumatic Conveying Conditions For Pellet Conveying

- **Some Heuristics...**

- ***Velocities***

- Pickup = 4,200 ft/min for pressure

- = 4,400 ft/min for vacuum***

- Terminal (exit) should be less than 6,000 ft/min

- ***Temperature***

- As cold as possible!

- Temperatures above 100 °F are excessive

Designing Line Layout

- Avoid inclined lines
 - *Keep lines horizontal and vertical*
- Avoid installing elbows within close distances to each other
 - *Have straight stretch between elbows*
- Avoid bends and use direct paths
- Avoid bends within 20-30 pipe diameters from the pickup point
- Never use more than 2 bends in a series
- Downward conveying design
 - *Treat as horizontal when doing pressure calculations*

Designs Which Cause Line Plugs

- **Line configurations**
 - ***Avoid bends at the pickup***
 - First bend at ~ 20-30 pipe diameters
 - ***Minimize the changes in direction***
 - ***Do not use upward sloping lines***
- **Conveying air conditions**
 - ***If a loss of air volume occurs, check...***
 - Blower: dirty filters, leakage through rotary feeders, valves, couplings, holes, non-seating RV, opening of RV due to over pressuring
 - ***Dirty filter on resin vessel***

Designs Which Cause Line Plugs

- **Miscellaneous**

- ***Resin vessel***

- Improperly sized feeder
 - bridging in cone

- ***Material buildup in line***

- result of fine materials and moisture
 - Additives, etc.

A line plug will typically be found about 40' downstream of a leak!!!

Ways To Increase Capacity

- Minimize flex hose length and eliminate where possible
- Increase pressure to system's maximum by optimizing solids/air ratio
- Check sloping lines for recycling of material
- Minimize the number of bends
- Shorten the total conveying distance
- Increase/decrease the system's air supply
 - *Install a larger/smaller blower, change rpm, etc*
 - *Must take into consideration pressure limitations*
- Step up the line diameter near the end of the system
 - *Doing so decreases the total system pressure*

Ways To Minimize Wear in Conveying Lines

- **Wear:**

$$\textit{Time to Failure} \propto (\textit{linear velocity})^{-4}$$

- **Reduce conveying velocities**

- **Use wear resistant materials**

- *More prevalent for abrasive materials*

- Sand, carbon black, etc.

- **Minimize line length and number of bends**

- *Lower velocities and fewer changes in direction*

Ways To Minimize Wear in Vessels

- **Enter the vessel radially, not tangentially**
- **Hang a flapper in the middle of the bin to allow the material to contact it instead of the vessel wall**
- **Step up the line diameter 40' before the vessel entrance to reduce conveying velocities**

Top 5 Reasons for Fines/Streamers Issues...

- 1. High transfer velocities**
- 2. High conveying temperatures**
 - *No cooler on pressure system*
- 3. Long Radius Bends in service**
 - *Especially near the end of a conveying system*
- 4. No fines/streamers removal device**
 - *Bag filter on vacuum suction*
- 5. No preventative maintenance for silo washing**
 - *Rinse out silos at least semi-annually*

Resources

- **Transfer System Engineering Companies**
 - ***MAC***
 - ***Hammertek***
 - ***Fuller Bulk Handling***
 - ***Coperion Waeschle***
- **Consultants**
 - ***Pneumatic conveying consultants: Paul Solt***
 - <http://www.powderandbulk.com/pcc/index.html>
 - Phone: (610) 437-3220 (pccsolt@itw.com)
 - ***PSRI (Particulate Solid Research, Inc.): Ted Knowlton***
 - <http://psrichicago.com/>
 - Phone: (773) 523-7227 (tmkspri@ix.netcom.com)
- **www.powderandbulk.com**
 - ***“Pneumatics Points to Ponder” Articles by Paul Solt***

Questions?

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